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Report No. 3 Contract No. DA-36-039-SC-90699 DA Project No. 3M-36-21-004-02

Third Quarterly Progress Report 1 January 1963 to 1 April 1963

to

U. S. Army Electronics Research and Development Laboratory Fort Monmouth, New Jersey

HYDROGEN GENERATION

FOR

HIGH ALTITUDE BALLOONS

31 May 1963

MSA Research Corporation

Subsidiary of Mine Safety Appliances Company

Callery, Pennsylvania

406 21

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HYDROGEN GENERATION FOR HIGH ALTITUDE BALLOONS

Report No. 3
Contract No. DA 36-039-SC-90699
Signal Corps Technical Requirement No. SCL-5743A
(26 September 1961)
DA Project No. 3M-36-21-004-02

MSAR XA-720318

Third Quarterly Progress Report 1 January 1963 to 1 April 1963

The objective of this contract is to study various hydrogen producing chemicals, evaluate their performance and the development of a design for a hydrogen generator suitable for inflation of high altitude balloons.

W. J. Carter R. A. Spencer M. J. McGoff

31 May 1963

MSA RESEARCH CORPORATION Callery, Pennsylvania

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PURPOSE

The purpose of the work under Contract DA-36-039-SC-90699 is to study various hydrogen generating systems, to design a hydrogen generator for high altitude balloons and to produce a test supply of charges for the U. S. Army. The U. S. Army has need of an economical and portable supply of hydrogen to inflate weather balloons in the field. Heretofore they have used a Hydrogen Generator Set AN/TMQ-3 and Calcium Hydride Charges ML-304/TM and ML-305/TM to inflate 800 gram neoprene ML-518 balloons. Design specifications outlined in accordance with the Signal Corps Technical Requirement SCL-5743-A require:

- (1) A chemical charge of NaBH4 or NaAH4 which will produce 45 SCF of H2 in 30 minutes and have a minimum shelf life of 10 years.
- (2) An expendable and economical container compatible with the 32 gallons or a maximum of 50 gallons of water, if desired.
- (3) The generator should have a capacity of 1 to 6 charges, and be equal to or smaller than the present AN/TMQ-3 generator.
- (4) The weight of the generator should be equal to or less than the present model, operate at low pressure, and be of a simple, rugged but safe design.
- (5) Hydrogen generation must be started within 10 minutes after setup and a balloon must be inflated within 30 minutes.
- (6) The new design should be capable of being cleaned and repacked or available for reuse within 15 minutes and should also produce 99% hydrogen evolved at temperatures below 140°F.

An outline of the test program is as follows:

1. Make a survey of the literature to determine the state of the art of generating hydrogen and the most promising and economical method of producing H₂ for high altitude balloons.

- Conduct laboratory scale tests to determine the best method of accelerating the reaction; water requirements; and the best antifoam agents, where required.
- 3. Make a preliminary design of a large scale generator to evaluate 45 cu ft charges to obtain engineering data.
- 4. Perform shelf life tests on the most promising chemical charges.
- 5. Make an evaluation of the large scale charges in the preliminary design generator to evaluate performance.
- 6. Make a final design of generator and prepare 50 NaBH4 and 50 NaAlH4 charges for submission to the U.S. Army Electronics Research and Development Laboratory.
- 7. Following approval of this model, fabricate two development model hydrogen generators and package 150 charges of NaBH4.
- 8. Prepare operation manuals and chemical specifications of the packaged charges.
- 9. Provide technical personnel to the U. S. Army Electronics Research and Development Laboratory during tests of the generator at Fort Monmouth.
- 10. Make monthly, quarterly and final reports in accordance with contract requirements as outlined.

ABSTRACT

During this report period, 1 January 1963 - 1 April 1963, ninety (90) small and large scale tests (up to 270 cu ft H₂ STP) were run. Data obtained from these tests enabled the design and packaging of fifty (50) NaBH₄, fifty (50) NaAlH₄ charges and the design and fabrication of a test model Hydrogen Generator (Model XI). The Generator and 100 charges were shipped to the U. S. Army Electronics Research and Development Laboratory.

MSAR personnel demonstrated the test model Hydrogen Generator on 29 March 1963. Two runs were conducted, each reacting three NaBH4 charges and evolving the required 135 cu ft $\rm H_2$.

Parameters investigated during this period included the forming pressure and physical packaging technique of large and small quantities of NaBH4; and the mixing of various amounts and combinations of catalysts. These efforts were primarily directed toward obtaining a uniform hydrogen generation rate from NaBH4. The best package developed was a 550 gm NaBH4 charge containing 40 gm LiH, 11 gm CoCl2 pressed in a 3 in. x 8 7/8 in. canister.

A uniform H_2 generation rate has been achieved with NaAlH₄.

Shelf life tests indicated NaBH₄ samples stored at 50°C gave lower yields than fresh control samples and required a longer time for H₂ evolution. The NaAlH₄ runs showed no significant differences from similar fresh controls.

REPORTS AND CONFERENCES

Within this report period, 1 January 1963 - 1 April 1963, the following reports were issued and conferences held.

Reports

- MSAR 63-17 Second Quarterly Progress Report
 "Hydrogen Generation for High Altitude Balloons"
 W. J. Carter, R. A. Spencer and M. J. McGoff
 26 February 1963
- 2. MSAR 63-27 Letter Report No. 5 "Hydrogen Generation for High Altitude Balloons" W. J. Carter and M. J. McGoff 4 February 1963
- 3. MSAR 63-45 Letter Report No. 6 "Hydrogen Generation for High Altitude Balloons" W. J. Carter and M. J. McGoff 4 March 1963
- 4. MSAR 63-50 Trip Report U. S. Army Electronics Research and Development Laboratory M. J. McGoff 25 March 1963

Conferences .

- 1. On 18 January 1963, at Callery, Pa., R. Welt of the U. S. Electronics Research and Development Laboratory conferred with MSAR personnel on progress of the project and problems anticipated in production of end items.
- 2. On 29 March 1963, at Fort Monmouth, New Jersey, a conference was held and the test model Hydrogen Generator was demonstrated.

EXPERIMENTAL

During this report period, 1 January 1963 - 1 April 1963, ninety (90) tests were made with NaBH4 and NaAlH4 charges. These were conducted in order to develop a charge canister, a generator and a packaging procedure that would evolve the desired amount of H2 in the required length of time (30 minutes).

The test methods and areas of investigation were as follows:

- Continued investigations of shelf life samples.
- 2. A series of runs using six (6) consecutive NaAlH4 charges in the same water.
- 3. Sizing the canisters.
- 4. Tests to corroborate the interpolation of small to large scale test.
- 5. Sizing the generator.
- 6. Steps taken to improve the reaction rate of the NaBH4 charge.
 - a. The use of wax or mineral oil combined with NaBH₄ in the lower portion of the charge.
 - b. A baffle plate with twenty 1/16 in. dia. holes and inserted near the bottom of the charge canister.
 - c. The application of different packaging pressure from the bottom to the top of the charge canister.
 - d. The variation of amounts and per cent of CoCl₂ mixed in the different stages of the charge.
 - e. The addition of LiH to the top layer to speed up H₂ evolution and, give a more predictable reaction time.

f. The use of more than one catalyst (AlSO4 and B2O3 with CoCl₂) to start the reaction.

A charge generates 45 cu ft H_2 measured at standard conditions of 0°C and 760 mm Hg and will be indicated as such in this report unless otherwise stated.

1. Laboratory Tests With NaBH4 and NaAlH4

Small scale tests with NaBH4 and NaAlH4 are tabulated in Table 1. Large scale test results with NaBH4 and NaAlH4 are listed in Table 2. Large scale tests are defined as those that generated 45-270 cu ft (STP) H2. Major emphasis during this report period was placed on large scale testing to evolve a suitable hydrogen charge and generator design for the Army which could generate up to 270 cu ft H2 in a 30 minute period.

Small Scale Tests With NaBH4

The small scale tests were run to investigate techniques to control H2 generation before advancing to full scale test charges. Data obtained from these runs which appeared promising was then used as information in packaging charges for large scale testing. Specificially, the concentration of the catalyst CoCl2 and forming pressures were surveyed in the small scale tests. It was found that small scale test data was limited in the applicability to large scale tests because of the NaBH4 behavior.

Small Scale Tests With NaAlH4

Small scale test data with NaAlH4 was found to be applicable to large scale tests. Extrapolation of small scale data was used to mock-up the large scale tests. Data for small scale tests with NaAlH4 is given in Table 1.

The primary problem with NaAlH4 has been the moderation of the reaction with water. Paraffin wax has been found to accomplish the moderation of the reaction but the wax must be melted in the mixing operation. To eliminate the melting of wax, mineral oil, a liquid at room temperature, was investigated as a possible moderating agent. A small scale run prepared with mineral oil did not effectively moderate the reaction as well as the paraffin wax.

A small scale test of six successive charges of NaAlH4 was run and data plotted in Fig. 1. The test was run in the laboratory test apparatus, in which the water temperature, H_2 temperature, and H_2 flow rate were recorded. As indicated by the

TABLE 1 - SMALL SCALE EXPERIMENTS WITH NaBH4 AND NaA1H4

	Hydride Pre Composition and Weight (g)	Cup Forming		Water			H2 Yi	e 1d	Elapsed	
Run No.		Diameter (mm)	Pressure (psi)	Volume (liters)	Temp. Start	End	liters at STP	Theor.	Time (min)	Romarks
154	NaBil4-118; CoCl2- 10	704	3,900	52 1/2	••		7,43	80.0	16	
155	NaA1H4-52; Wax-10	272	11,350	1	20	81	2.29	92.0	12	
156	NaA1114-25; wax-5	45 '	3,200	2	31	58	1.31	89.0	3.7	Six (6) consecutive charges
		45	!		33	\$5	1.31	89.0	3.7	added to some water,
		45	į	•	54	71	1.31	89.0	6.0	Water cooled before second
		45		-	65	79	1.31	89.0	3.5	and sixth cups were added.
		45	į	•	76	86	1.36	91.6	4.5	
	τ	45	\	-	32	\$6	1.31	89.0	3.8	
157	NaA1114-25; Wax-5	27	3,400	1	20	64	1.33	90.0	6.5	
158		27	6,800	1	19	58	1.34	90.0	8.5	
159	•	27	11,350	1	20	66	1.30	89.0	7.0	
160	NaA1H4-48; Wax-9.5	27	3,400	2	19	52	2.09	92.5	10.0	
161	NaA1114-54; Wax-10.8	27	3,400	4	20	39	2.36	93.0	9.8	
162	\dagger	27	6,800	2	18	58	2.37	93.5	12,8	
163	NaA1H4-52; Wax-10.4	27	13,600	4	16	36	2.24	92.0	12.8	
164	NaA1H4-50; Wax-10.0	42.53	2,140	2	22	63	2.68	91.5	4.1	
165	NaBH4-50; CoC12-4	42.5	1,780	3	16	45	3.74	90.0	11.7	
166		42.5	1,780	2	20	54	3.85	92.0	8.0	
167	NaBII4-25; CoC12-4	45	3,200	ı	18	35	0.80	38.0	16.0	Used sea water, low yield
168		45	1	1	16	49	1.85	88.5	12.0	Control tap water
169		45		1	19	39	1.25	59.9	35.0	Used sea water
195	NaBil4-25; NaAlil4-2.5	45	ţ	1			••	••	••	No catalyst, only NaAlH ₄ reacted
98-205	NaBH4-25; CoC12	45	_	1	••		••			Small scale samples pack- aged to duplicate large scale test. Result did not
221	NaAlH4-25; Mineral Oil-3.8	45	3,200	1	22	63	1.08	72.0	1.8	duplicate large scale test.

45 mm cup; surface area 15.90 sq cm 27 mm cup; surface area 5.72 sq cm 42.5 mm cup; surface area 14.25 sq cm 70 mm cup; surface area 38.5 sq cm

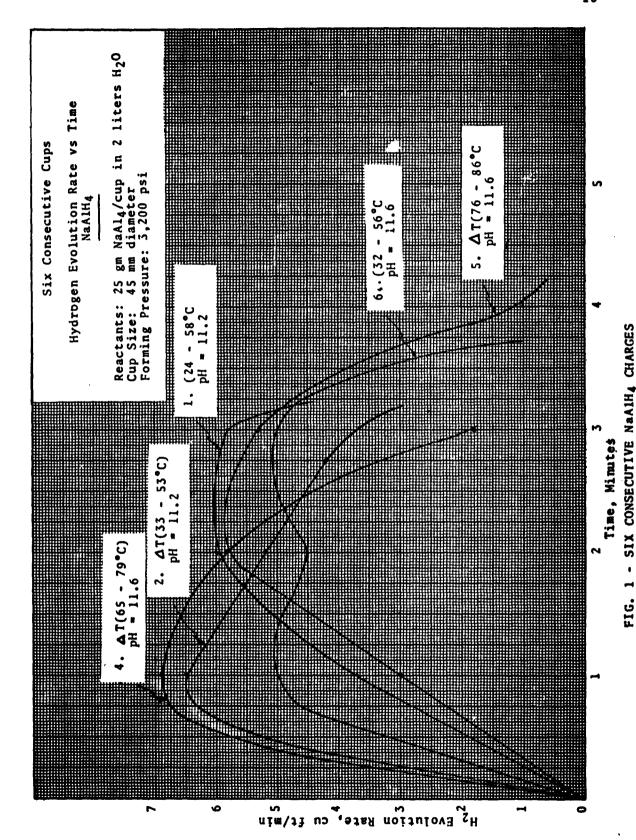
TABLE 2 - LARGE SCALE HYDROGEN GENERATION FROM NaBH4 AND NaAlH4

	COMPOSITIO	liyd n & Welght	ride Prepara Number	Cup	Forming		Water		H ₂ Yi	•ld	Elapsed	
n	(g		of Canisters	Diam.	Pressure psi	Volume (Gal)	Temp Initial	(°C) Final	cu ft at STP	Theor.	Time (min)	Rows
70 71	600 NaBil4	52 CoC1 ₂	one	(18)	3,400 3,400	6 6	15 16	51 53	43.4 46.2	87.0 92.5	8 8	
72	600	48			4,000	6	25	28	46.0	92.0	46	
73	600	144	three		1	18 6	21	40	•	:	11.5	(1 (2
74 75	600	48 24	ohe 1			ů	22 20	55	-	-	21.0	
76	1	16	ļ.		i		21	56	.: .		25.9	(3
77 78		16 48	1		ĺ	1	21 21	55	45.5	91.0		(4
79	Ţ	14	1		ļ	1	13	48	46.3	92.5	72	•
80 81	200	12 16			j		20	54	46.0	92.0	58	
2.1	400	10	*		ļ	L	21	5.5	47.0	94.0	37	
8 2	200	16	Two		1							
8.3	400 200	0 16	three		1	12.7	20	5 2	95.0	91.3	46	(:
	400	0			- 1	17.0	22	59	137.0	91.5	39.5	(
84	200	16	one		İ	6	21	54	45.6	91.2	48.0	(
8 5	400 250	0 20	1		- 1		21	34	43.0	91.2	40.0	,,
	350	0	i		!	6	22	55	45.8	91.6	36.9	
86	200 400	16 0			l	6	21	54	45.2	90.5	59	C
87	300	24	Į.		ı			-				•
88	300 200	0 16	ı		l	6	21	55	45.1	90.2	27	
	200	0	1		l							_
89	200 300	40 Wax	1			6	21	53	44.5	89.0	50	(
9	300	24 CoCl ₂ 45 Wax	1		ł	6	21	38	25.7	45.0	16	C
90	300	24 CoCl ₂			l		• •			01.4	••	
91	300 300	45 Wax 24 CoCl ₂				4	21	67	45.9	91.6	33	
	150	0 -				_						
9 2	150 300	22.5 Wax 24 CoCl ₂	ł		- 1	5	20	60	45.4	90.6	19.3	
-	200	0 -	1		ĺ							
93	100 300	15 Wax 24 CoCl ₂	ł		1	6	21	54	44.4	87.2	32	
,,	100	0 00017	- 1		1							
	200	Below a				6	21	56	45.6	91.2	19.5	
94	200	baffle pl 16 CoCl ₂	ate	To	p 2,500							
	100	0 -	1	Cente	er "	_						
96	300 250	0 20 CoCl ₂	1	Botte	om 5,000	6	21	55	44.6	89.4	35.5	
-	150	0 -	l.		ŀ						•• •	
	200	Below a baffle pl	,,, V		. ↓	5.3	20	58	43.1	86.5	39.2	
97	250	20 CoC12	Six	To	ορ 2,000							
18	350 250	0 20 CoC1 ₂	~	Botte	om 5,000	3 2	19	58	272	90.0	22.6	-(C
- 0	150	0 -	One I	Te	ор 2,000							
19	200 250	20 minera 20 CoCl ₂	1 011	Botte	om 5,450	6	20	51	46.2	92.4	38	
	350	0 -	i	Botte	op 2,500 om 5,450	6	10	47	45.6	91.2	44	
20	200	8 CoCl ₂	Ţ	To	op 3,000							
22	400 250	0 20 CoCl ₂	Six	BOTT:	om 5,450 op 4,000	6	20	55	45.8	91.6	59	ĺ
	350	0 -		Botte	om 4,000	6	20	56	274	91.5	29.9	(1
23	200	50 Lill4 11 CoCl ₂	One		op 4,000 om 5,450	6	21	S 9	48.4	96.0	30.5	
	350	0 00012	•	2000	0,700	•			74.7			

TABLE 2 - LARGE SCALE HYDROGEN GENERATION FROM NaBH4 AND NaA1H4 (cont)

(274	825 NEALHA	140 Wax	5,450	8	22	71	45.5	94.0	25	
)	225	200 NaBila	50 Lill	Top 4,000	6	22 21.5	71 60.5	45.7	95.0	26.3	
١.		•	11 CoCl ₂	i							
		350	0		6	21	60	45.7	95.0	26.5	
	226	200	40 Lill	Six Top 4,000							
1			11 CoCl2	B B 488			• -	200		••	(12)
1		350	0	Bottom 5,450	36 27	17 21	56 63	280	93.4 90.0	31 28	(12)
1.	227 231	825 Na/1114 540 NaBH4	140 Wax 50 Lill	Three 5,450 310 gm NaBH4 on bottom	21	21	03	135	90.0	40	
	-31	340 Manil	8 Wax	heated to 100°C 2 hrs							
			10 CoC12	pressed to 15,000 psig.	6	21	60	46.6 ft	3	24	
				Balance of charge	•	•-					
1				pressed to 10,000 psig							
1	232	575 NaBlt₄	25 Lill	25 gm Lill placed between							
٠.		•	16 CoCl ₂	175 gm NaBH4 and 200 gm					1		
				NaBil4 pressed to	6	21	58	48.0 ft	•	32	(13)
4 -				14,000 psig. Top 200 gm							
1	233	550 N-00	40.0.0	NaBil4 pressed to 6,000 psig							
1	233	550 NaBH4	40 B ₂ O ₃ 11 CoCl ₂	350 gm NaBH4 on bottom 14,000 psig. Balance on	6	21	53			35.7	(14)
1			11 00012	top pressed to 7,000 psig	U	21	33			33.7	(14)
	234	550	40 LiH	(See Run No. 228)	6	21	46			60	(15)
	•••	•••	11 CoCl,	(500 11411 1151 225)	•						,,
(235	550 NaBH.	40 1.111	(See Run No. 228)	6	21	58			36	(1ϵ)
1		•	ll CoCl,	-							
٤.	236	550	40 L111								
			11 CoCl ₂	(See Ran No. 228)	6	21	44			60	(17)

(1) Reaction became violent after 15 min.
(2) Repeat of Run 173. Foamed out of 10 gal. container inside a 30 gal. drum.
(3) Meter failed during run.
(4) Baffle plate on top of canister.
(5) Canister in vertical position.
(6) Canister in horizontal position.
(7) Same HyO as Run 185.
(8) Max slowed reaction down.
(9) Stopped at wax.
(10) Foam.
(11) 1075 ml Foam and condensate.
(12) 263 cc foam and condensate.
(12) 263 cc foam and condensate.
(13) Lill reacted as expected at 26 min. Hy evolution rate increased from 1 ft³/min to \$5.8 ft³/min.
(14) ByOs boric anhydride gave smooth Hy evolution. No accoleration of reaction near end.
(15) Rün outside in ~0°C atmosphere open drum to observe foam ~ ~5 in.
(16) Repeat of above except drum was insulated. Foam ~ 5 in.
(17) Used 240 ml gum turpentine, 80 ml aniline. Reduced foam to less than 1 in. Note: slow reaction time, also obnoxious vapor.
(18) 4 3/4 in. diameter cup used in Runs 170 and 171, all other runs used a standard 3 in. diameter canister.



聖ををからだって、 こ

curves, NaAlH4 charges can be run in succession using the same reaction water (pH 11.7) with very little difference in H2 rate reaction. Some of these charges were run at higher initial starting temperatures. The higher temperatures (24° - 76° C) also had little effect on the H2 reaction rate.

Large Scale Tests With NaBH4

Table 2 lists data obtained on large scale tests with NaBH4.

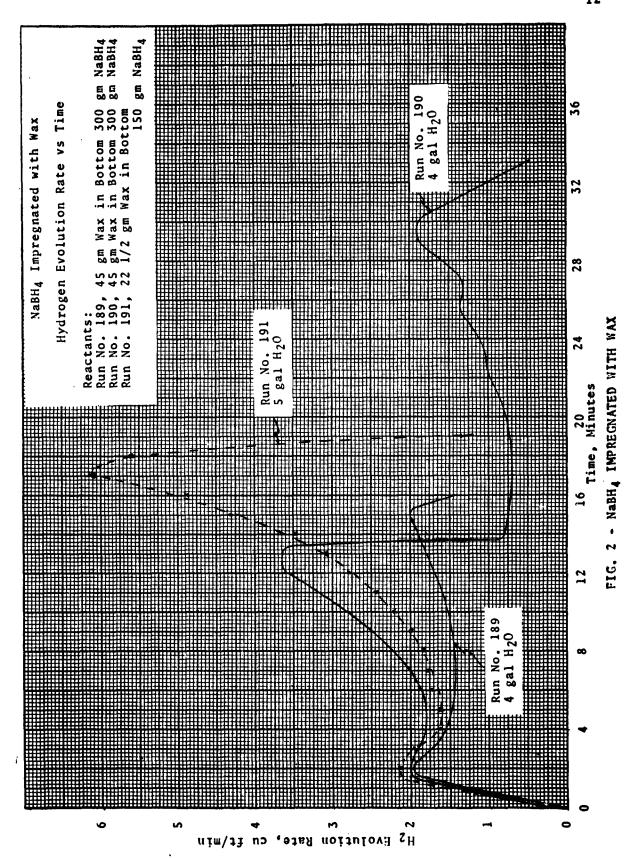
Various techniques were examined in an effort to promote uniform hydrogen generation with NaBH4. One of the major problems in generating H2 with NaBH4 is the formation of foam. Foam is a function of instantaneous H2 generation rate. If generation rate is too rapid, excessive foaming results thus requiring a large free volume to contain the reaction. Therefore, a major solution to development of a suitable hydrogen generation using NaBH4 lies in the techniques of packaging NaBH4 to give a uniform H2 evolution rate. The following techniques have been explored in large scale tests to develop a uniform H2 generation rate with a minimum formation of foam.

These approaches have been:

- a. The use of wax and mineral oil
- b. Baffle plate
- c. Application of different packaging pressure
- d. Varying the amount of CoCl2
- e. Seeding NaBH4 charge with LiH
- f. Combination of other catalysts with CoCl₂

a. The Use of Wax and Mineral Oil

A number of charges were run in which mineral oil or wax was incorporated into the charge. This was suggested as a means of forming a partial barrier to slow down the accelerating reaction which takes place in the last half of the charge. As can be seen in Fig. 2, Run No. 189, the wax completely stopped the reaction with 50% of the H2 evolved. A subsequent charge Run No. 190 was run in which less water was used in order to increase the temperature of the water so that the wax would melt. On



Tours of the

reacting this charge, the reaction rate was slowed up at the wax front (after 14 minutes) and then proceeded to accelerate again. Temperatures were 26°F higher when the wax barrier was encountered. A third charge was (Run No. 191) run in which the wax was pressed in the bottom quarter of the charge. On reaction of this charge, the wax had no visible effect on the H2 evolution rate. Mineral oil was used in Run No. 218; 200 gm was mixed and pressed with the bottom 1/3 of the charge. On reaction of this charge, the decelerating effect was too long; i.e., after 30 minutes. In view of these results, no further work was done to incorporate the wax or mineral oil into the NaBH4 charge.

b. Baffle Plate

A baffle plate with twenty 1/16 in dia holes was placed 1/3 of the way up from the bottom of the charge canister. It was anticipated that the decreased area would limit the amount of water present at the reacting chemical front. On reacting the charge, there was not visible difference between this and a standard canister, so effort along this line was discontinued.

c. Application of Different Packaging Pressures

A number of experiments were run in which the forming pressure of the charge was varied from 1,000 to 6,000 psi. Data from these runs indicated that the higher forming pressures tend to give longer reaction time. The data obtained looked promising enough that further work using higher pressures or hot pressing the material would be worthy of consideration.

d. Varying the Amount of Cobalt Chloride

A new approach was required to slow down the prohibitively fast reaction caused by a NaBH4 charge packaged with 8% CoCl2 and reacted in 6 gal of water. Fig. 3 shows two characteristic type curves: One curve is a NaBH4 charge having 8% CoCl2 (a total of 48 g) mixed with the charge and the other is a NaBH4 charge having 8% CoCl2 (a total of 16 g) mixed with the top 200 gm NaBH4. Experiments were set up to study the effects of varying the per cent of COCl2 mixed with the top portion of the charge. The data obtained indicated that even for identical charges, time required for reaction was very unpredictable, with as much as 25 minutes variation in reaction time.

e. Seeding NaBH4 Charge with LiH

In order to develop a more predictable charge, it was theorized that a highly active hydride material could be seeded with the NaBH4 to disperse the CoCl₂ more quickly in the reaction water.

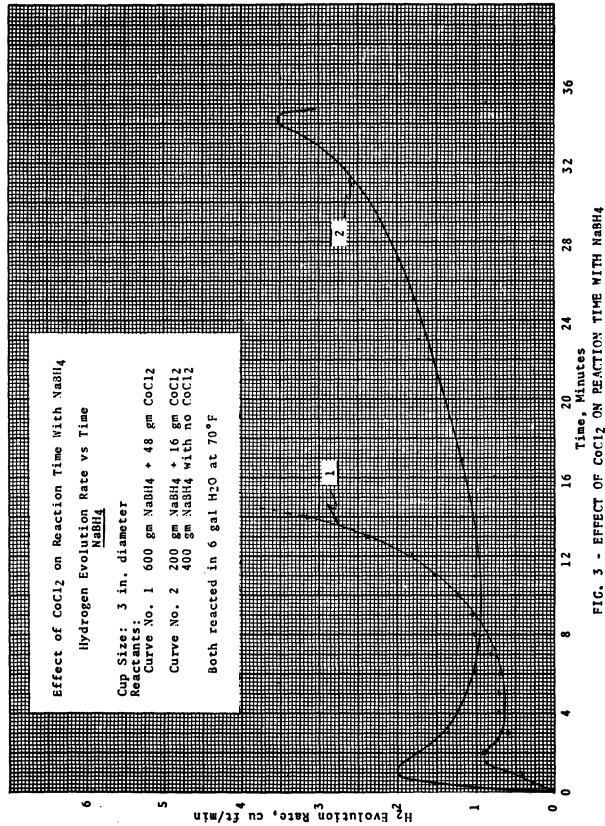


FIG. 3 - EFFECT OF COC12 ON PEACTION TIME WITH NABH4

Pot make

The top portion of the NaBH4 charge was seeded with LiH which was selected because of its high available yield of H2 per unit weight. Fig. 4 shows two of these charges seeded with 50 gm of LiH and reacted in a sealed H2 generator using 6 gal of water at temperatures of 70°F . The total time of reaction of this type charge has been predictable within \pm 3 minutes.

f. Combination of Other Catalysts With CoCl2

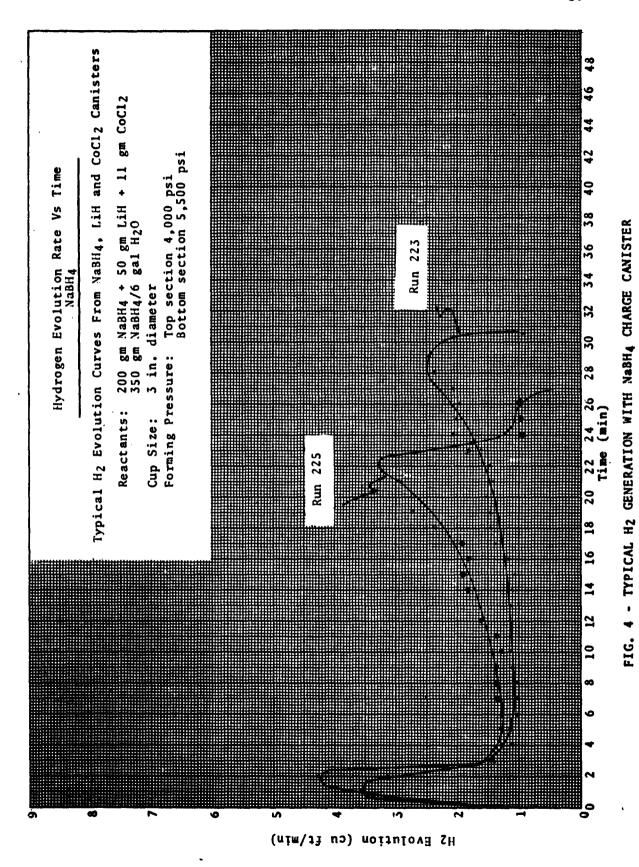
One test was conducted using boric oxide and CoCl2 mixed and compressed with the NaBH4 charge. As shown on Fig. 5, the behavior of the charge with boric oxide has a somewhat more uniform H2 generation reaction without greatly altering the total reaction time or reducing the yield. In view of the results, it is felt that further work on mixing of different types of catalysts would provide more uniform H2 evolution rates.

One test was run using 4% aluminum sulfate (8 gm) and 4% cobalt chloride (8 gm) mixed with the top 200 gm of NaBH4. On reacting the charge, the $\rm H_2$ evolution rate curve was very similar to that of a straight CoCl₂ catalyst charge. This similar reaction rate was attributed to the low per cent of AlSO₄ initially packaged with the charge.

The behavior of the hydrolysis reaction of a solid NaBH4 charge was examined in other runs. One experiment was set up to check whether a NaBH4 charge packaged in a 3 in. dia. canister reacted as a moving front or is the NaBH4 dissolved out into the water after a short period of time. The test canister was packaged first pressing 175 gm NaBH4 in the bottom followed by a 25 gm section of LiH, then 200 gm NaBH4 and on top 200 gm NaBH4 and 16 gm CoCl2 mixture. Thus, the section of LiH was located 2/3 from the top of the charge. As shown on Fig. 6, a vertical line crossing the H2 rate curve is the theoretical point at which 66% of the available H2 has been evolved. The H2 evolution rate curve indicates that the LiH is reacting at this point and that the NaBH4 dissolves as a moving front through the charge.

One of the disadvantages in the use of NaBH4 for the generation of hydrogen is the tendency of the reacting solution to form a varied volume of foam. This formation of foam is peculiar to the borohydride among the different materials tested for use in H2 generation; however, it may be tied in with the fact that of these materials, only the borohydride dissolves in water prior to reacting.

In other experiments, a NaBH4 charge was reacted in an open container to observe foam formation. The foam appeared shortly after the start of the reaction. Small bubbles completely covered the water surface and were dispersed after reaching a



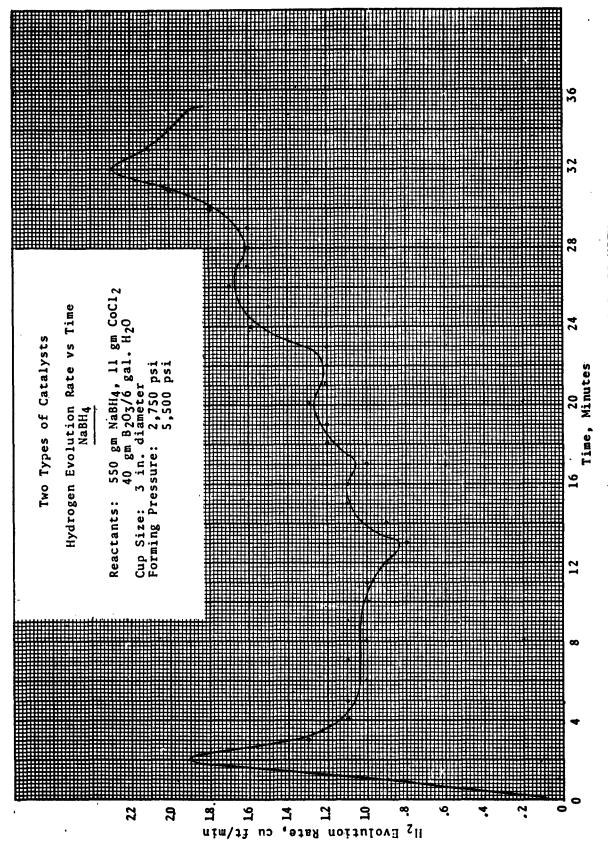
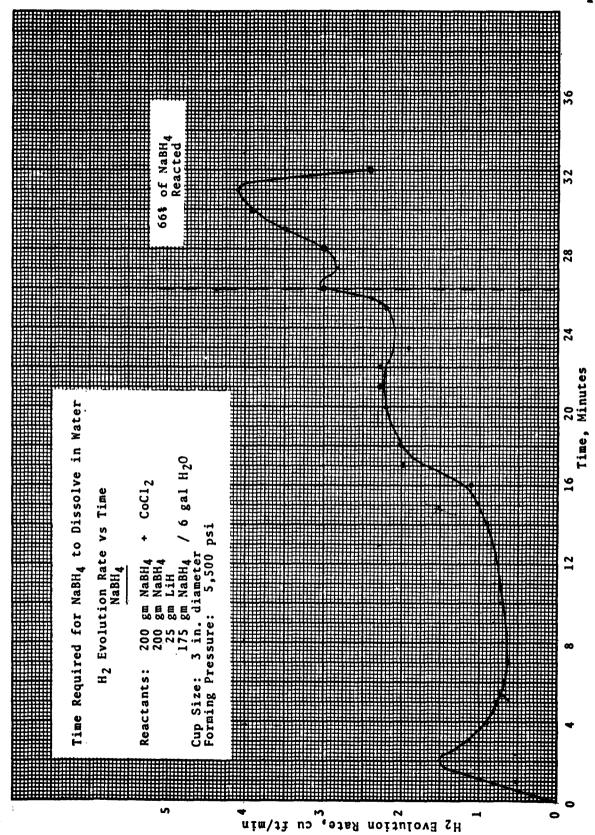


FIG. 5 - GENERATION OF H₂ WITH NaBH₄ BLENDED WITH COC12 and B₂O₃ CATALYSTS

FIG. 6 - TIME REQUIRED FOR NABH4 TO DISSOLVE IN WATER



diameter of approximately 1/2 in. These bubbles look and acted similar to those found in soapsuds. In several of the open foam experiments, black particles (believed to be cobalt boride) about the size of a pin head were observed floating and being agitated on the foam. As the reaction progressed, the bubbles continually increased in diameter before dispersing.

Three runs were analyzed to determine the maximum amount of foam produced at any time during; one (1) charge, three (3) charges, and six (6) charges. This data is plotted in Fig. 7 and indicates that the foam has a tendency to increase as the amount of the charge material is increased. Fig. 8 shows a comparison between volume of foam and rate of H_2 evolved and that a corollary relationship exists.

No tests were run to maintain a constant water temperature in the generator because it was felt that a field generator held at a constant temperature would not be practical. Therefore, the mixtures were allowed to heat up as the reaction proceeded.

Initial water temperature has an effect on reaction time with NaBH4. The observed effect is most prominent in the range below 20°C. This is illustrated in Fig. 9 where two identical charges were packaged, one was reacted in 6 gal of water with an initial temperature of 10°C and the other in 6 gal of water with an initial temperature of 21°C. About 8 minutes longer reaction time was noted in the run with 10°C water.

On 28 February 1963, fifty (50) NaBH4 charges were supplied to the U. S. Army Electronics Research and Development Laboratory. The generation of six (6) NaBH4 charges (the same formulation of those supplied) reacted with 36 gal of water is shown in Fig. 10. This generation curve is typical of the NaBH4 charges whether it be one charge with six (6) gal of water or three (3) charges with eighteen (18) gal of water at initial water temperature of 20°C. There is an initial high generation rate of H2, a slow down, and then an accelerating effect as the reaction proceeds to completion.

Large Scale NaAlH4 Tests

Small scale data on NaAlH4 runs were successfully applied to mock-up large scale tests with NaAlH4. The major problem encountered with NaAlH4 has been in moderating the reaction with water. This has been solved by blending the NaAlH4 with paraffin wax and controlling the surface exposed to reaction with water. Two large scale runs were performed with NaAlH4 and these tests illustrated that a uniform H2 generation in the specified 30 minutes is obtained. Fig. 11 shows the characteristic generation rate of NaAlH4 for a single 45 cu ft H2 charge. The

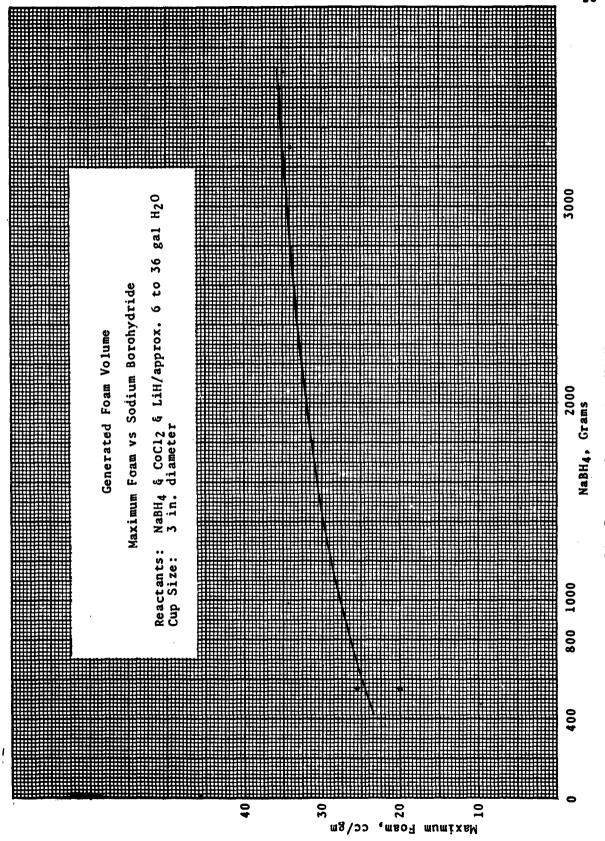
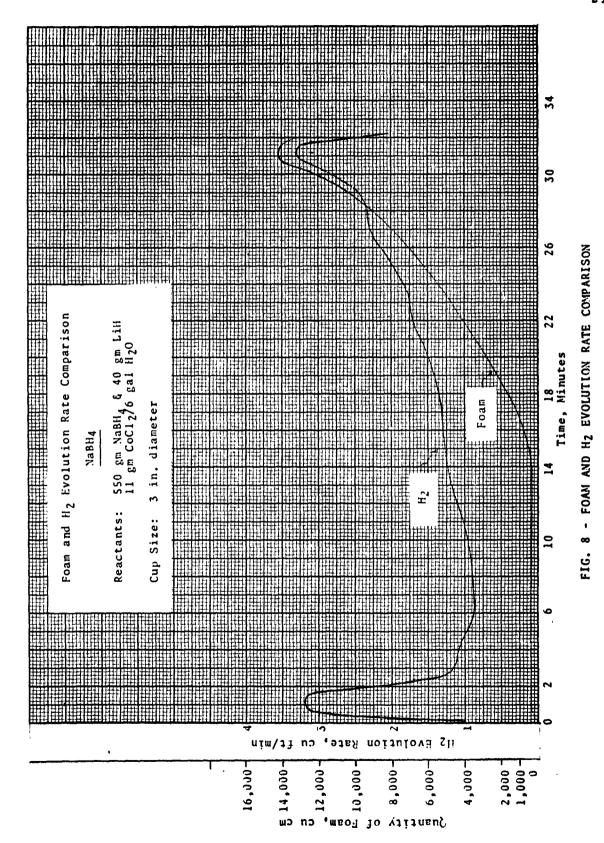
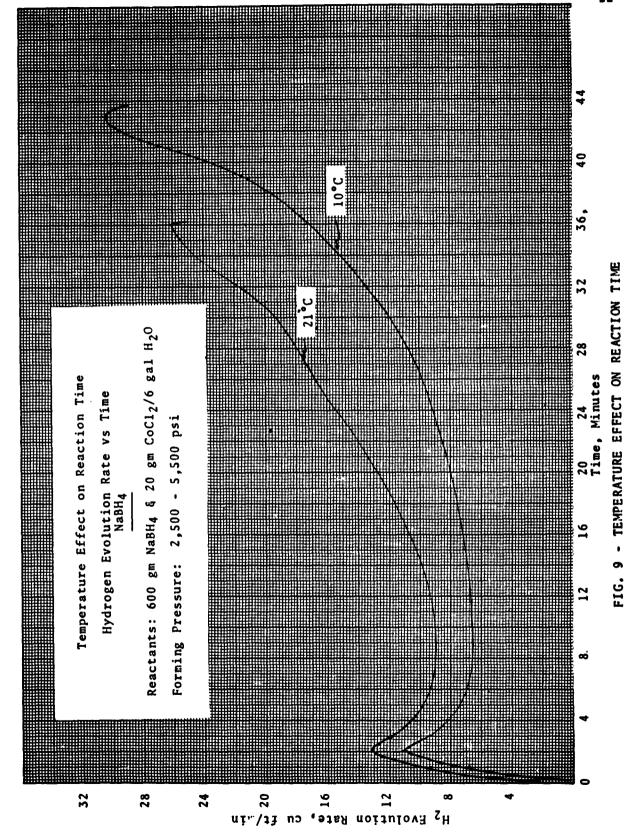
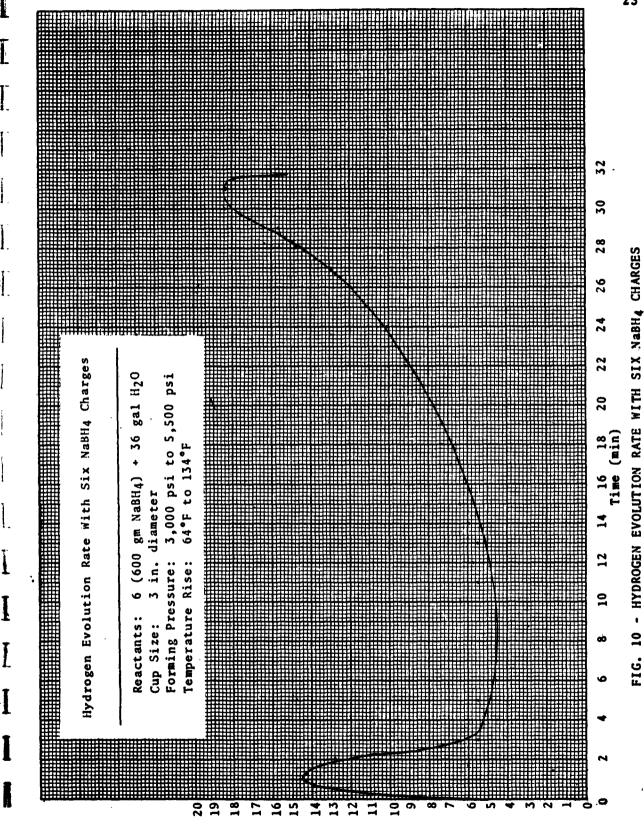


FIG. 7 - GENERATED FOAM VOLUME





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II2 Evolved (cu ft/min)

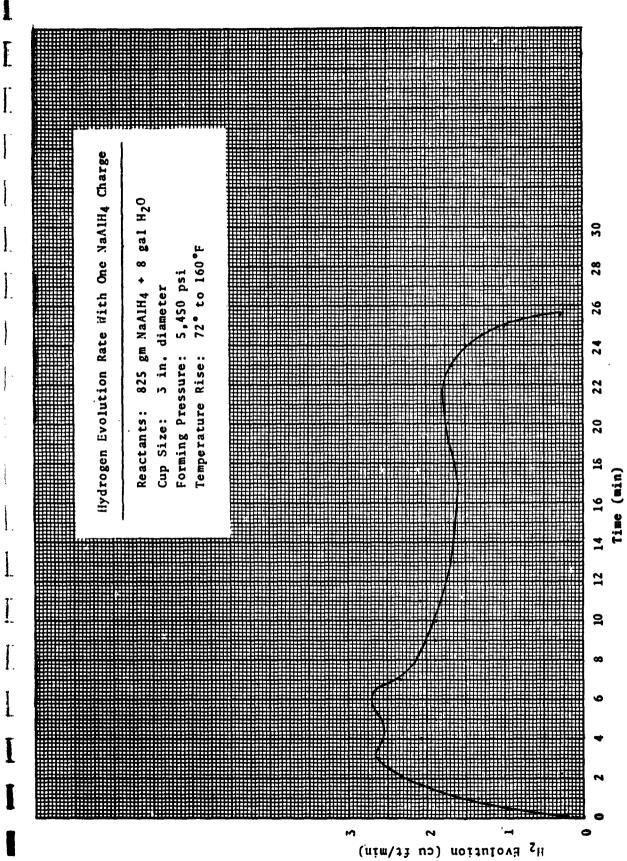


FIG. 11 - HYDROGEN EVOLUTION RATE NITH ONE NAAIH4 CHARGE

second large scale NaAlH4 run was made using three (3) 45 cu ft (STP) H2 charges (or a total of 135 cu ft H2 at STP) in the AN/TMQ-3 Generator. The NaAlH4 charges supplied to U. S. Army Electronics Research and Development Laboratory on 28 February 1963 can be used in the experimental generator (Model XI) supplied on that date or in the AN/TMQ-3 Generator.

On 28 February 1963, six (6) NaAlH4 charges were shipped to the USAELRDL. A total of fifty (50) charges were scheduled, but because of delay in receipt of NaAlH4 the remaining forty-four (44) charges were not packaged until 29 March 1963.

2. Shelf Life Tests

The shelf life tests were continued on both the NaBH4 and NaAlH4. The data obtained is tabulated in Table 3.

Samples of NaBH4 and NaAlH4 have been packaged in pellet and cup form for shelf life evaluation. Additional full scale NaBH4 charges; i.e., 45 cu ft H2 rated charges, have been packaged and are being evaluated for shelf life.

 $$\operatorname{NaBH4}$$ - Samples of 50 gm NaBH4, stored for three (3) months at $20\,^{\circ}\text{C}$ were evaluated and found to yield equivalent amounts of H2 but required slightly longer times for reaction.

Cups containing 25 gm NaBH4 at 20°C for three (3) months gave slightly lower yields (3%), in slightly longer periods. However, samples stored at 50°C in an oil bath gave significantly lower yields, 30% less and required three times as long for reaction. From these results it appears that storage at elevated temperature may adversely affect NaBH4.

However, when samples packaged in canisters in the manner supplied to the U. S. Electronics Research and Development Laboratory were examined for this effect, it was found that by reducing the amount of water used in the reaction, yield was unaffected and reaction time could be reduced. The charge containing 550 gm NaBH4, 40 gm LiH, and 11 gm CoCl2 when stored in oil at 100°C for 46 hours gave an equivalent yield as the fresh control sample but required almost twice the reaction time. When an identical sample was stored at 100°C for 113 hours and reacted in 4 gal of water instead of 6 gal, an equivalent yield was obtained in about 60% the reaction time of the control; i.e., 19 1/2 minutes instead of 32 minutes.

From these results, it appears the effect of prolonged storage at elevated temperatures may require less water or some agitation of the packaged material to enable the NaBH4, which may be caked to dissolve faster in the water.

TABLE 3 - SHELF LIFE TESTS WITH NaBH4 AND NaAlH4

Composition and Weight (g)	de Prepara Stora	ge	Form	Forming		ter	- °C	Elapsed Time	Yiel liters	d Theor.		
n •	Time (months)	(°C)		Volumo (liters)	Start	End	(min)	at STP	(1)	Remarks		
7 NAAliig=73	0	••	Pellet		2.9	22	59	3.0	4.25	99.1	Control Run	
8	0	••	Pellet	••	2.9	24	58	3.0	4.66		Control Run	
9	3	20	Pellet	••	2.9	24	66	2.0	3,25	76.0		
u	3	20	Pellet		2.9	22	60	2.5	4.03	94.0		
2 N#A1H4-25	0		Cup	60004	1.0	23	65	2.1	1.26	83.5	Control Run	
3	0		Cup	6000	1.0	23	.64	2.5	1.32	89.5	Control Run	
4	3	20	Cup	6000	1.0	20	60	3.1	1.32	89.5		
5	3	20	Cup	6000	1.0	23	62	3.5	1.37	92.5		
6 '	3	50	Cup	6000	1.0	15	63	4.2	1.32	89.5		
7	3	50	Cup	6000	1.0	23	63	3.1	1.30	88.0		
1 N#BH4-50; CoC12-4	3	20	Peliet	10,000	1.9	25	59	7.7	3,59	85.0		
2	3	20	Pellet	10,000	1.9	22	58	9.5	3.71	88.0		
3	0		Pellet	10,000	1.9	20	54	7.3	3.50	83.0	Control Run	
6 NaBil4-50; CoCl2 -2.2	0	••	Cup	6000	1.0	21	\$6	6.9	1.87	89.0	Control Run	
7	0		Cup	6000	1.0	21	55	9.0	1.85	89.0	Control Run	
8	3	20	Cup	6000	1.0	21	\$\$	9.0	1.81	86.0		
g e	3,	20	Cup	6000	1.0	22	55	8.5	1.78	85.2		
10	3	50	Cup	6000	1.0	21	53	24.5	1.15	55.0		
ı 	3	50	Cup	6000	1.0	21	51	22.2	1.23	59.0		
8 ¹ NaBH4-550; CoCl ₂ -11; LiH-40	46 hr	100	Cup	6000/14,000	22,72	20	53	55.0	46.03	92.0	Accelerated 100°C Stora	
9		• •	Cup	6000/14,000	22.7	20	57	32.0	46.0 ³	92.0	Control Run	
so †	113 hr	100	Cup	6000/14,000	22.7	20	70	19.5	46.0 ³	92.0		

Note: .1 2 3 4

Charges in Runs 228-230 typical of those furnished to USERDI, on 28 February 1963. Note 22.7 liters equals 6 gal.
Cubic feet.

A gage pressure of 6,000 psig gives a forming pressure of 1,900 psi.on the material as its pressed in a 45 mm diameter cup.

A gage pressure of 14,000 psig gives a forming pressure of 4,500 psi on the material as its pressed in a 45 mm diameter cup.

Ţ

This difficulty with the NaBH4 charge as packaged in a can requires further investigation.

NaAlH4 - Three month shelf samples of NaAlH4 in pellets and pressed cups stored at 20°C and in an oil bath at 50°C continue to show no significant difference from fresh control samples. This would indicate that storing of NaAlH4 at elevated temperatures has no significant effect on its shelf life. Additional samples of NaAlH4 packaged in sealed cans will be evaluated for shelf life when sufficient material is on hand.

3. Apparatus Design

The purpose of all experimentation has been to evolve a system which utilizes NaBH4 and NaAlH4 to generate H2 for inflating high altitude balloons. Both NaBH4 and NaAlH4 will generate more H2 per unit weight than CaH2 which is currently being used. However, the problems associated with NaBH4 and NaAlH4 and the relative material cost must be considered in the selection of a suitable material for future use by the Army.

A method of packaging NaBH4 and NaAlH4 has resulted from this work. A description of these designs follows. It has not been possible to reduce the size of the generator from the size of the AN/TMQ-3. This is because of the problem of foam associated with the use of NaBH4. Foaming has been materially reduced, through packaging techniques, and review of the literature indicates that foam has been reduced over that encountered by previous experimenters.*

In the development of the canisters, direction of design pertained to assembly of standard types of packaging even though the characteristics of H2 generation with NaBH4 is adversely affected by conditions such as quantity, temperature and types of water (fresh as compared to saline). The programing of the H2 generation with NaBH4 and NaAlH4 has also been directed to make both packages react within the specified 30 minute time period. Both materials were packaged in 3 in. dia. canisters, this being considered as the optimum size.

Canister Design

The dimensions of the canister were arrived at by projecting the small scale test into a large scale basis. A curve was constructed which indicated that a 5 in. dia. canister

^{*} The Generation of Hydrogen from Sodium Borohydride Ethyl Corporation, 30 December 1944.

would be required for the reaction of NaBH4 to evolve 45 cu ft H2 at STP from a single charge in a time of 25 minutes.

A 4 3/4 in. dia. mold was used to package two (2) test canisters (4 3/4 in. dia. x 3 1/4 in. high). The water used to react the NaBH4 was reduced from twelve (12) to six (6) gal per each 45 cu ft charge. The water was reduced to stay within the specifications of the contract (less than 50 gal of water for 270 cu ft H2). The reaction time for both of these test canisters was approximately 8 minute and the H2 was evolved at an excessive, accelerating rate. The data was taken from these runs and plotted on log log paper as surface area (sq cm) vs grams reacted per minute. The new canister size was predicted from this curve at 3.14 in. dia., but rounded off to 3 in. which was considered the minimum size dia. that could be used for both the NaBH4 and NaAlH4 canister. This was due to the restriction of the adapter used to connect the NaAlH4 charges in the AN/TMQ-3 Generator.

The results from the testing of the 3 in. dia. cups with NaBH4 were not satisfactory, because of the continued excessive accelerating affect from the CoCl2 as the reaction proceeded through the length of the charge. At this point, the amount of CoCl2 was reduced (discussed previously) to lessen the accelerating affect.

The canisters to hold both NaBH4 and NaAlH4 charges were specified and fabricated as shown on Fig. 12 and 13, respectively.

The NaBH4 charge canister contains 550 gm NaBH4, 40 gm LiH and 11 gm CoCl₂ and is pressed in two stages, top at 2,750 psi and the bottom at 5,500 psi. This charge is operable in only the MSAR Model XI Hydrogen Generator (See Fig. 14).

The NaAlH4 charge canister contains 825 gm NaAlH4, 140 gm wax and pressed at 5,500 psi and is operable in both the AN/TMQ-3 and the MSAR Model XI Hydrogen Generator.

Generator Design

The preliminary design and fabrication of the generator was completed on 28 February 1963 and shipped to the U.S. Army Electronics Research and Development Laboratory, Fort Monmouth, New Jersey.

The specifications given in the Army Technical Requirements SCL-5743-A are listed in a section of this report, (See Purpose). The design and shape of the generator also took into consideration: compactness, ease of operation, temperature of evolved hydrogen, ease of assembly and disassembly and the maximum amount of evolved hydrogen.

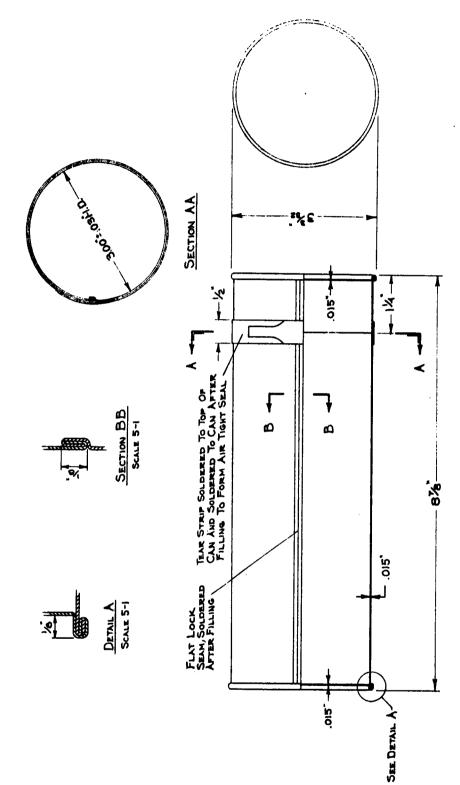
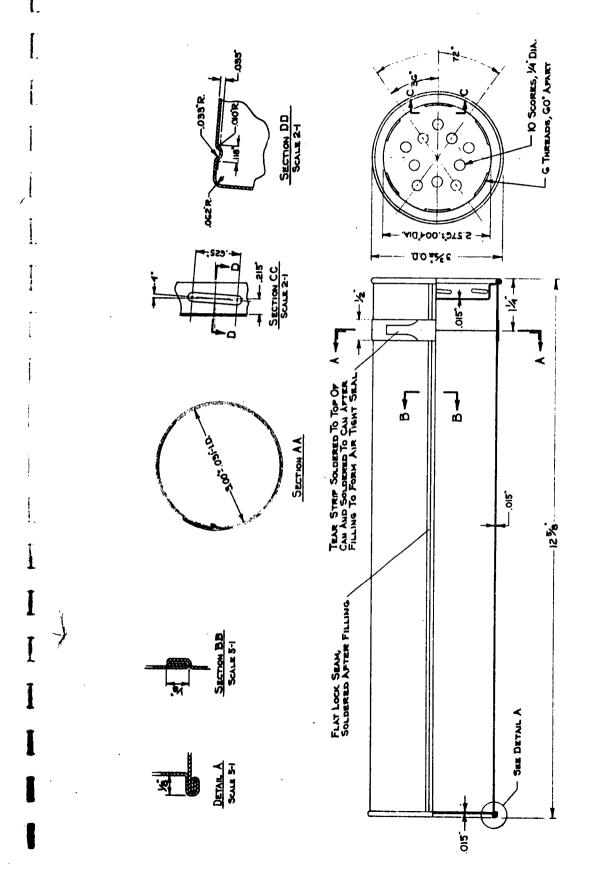


FIG. 12 - NaBH4 CANISTER

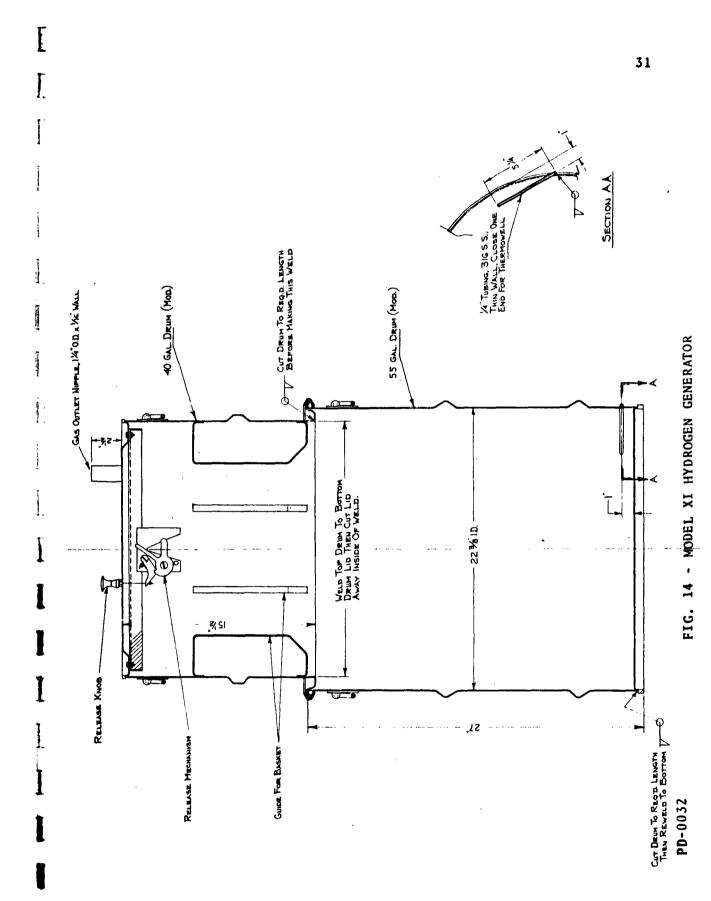
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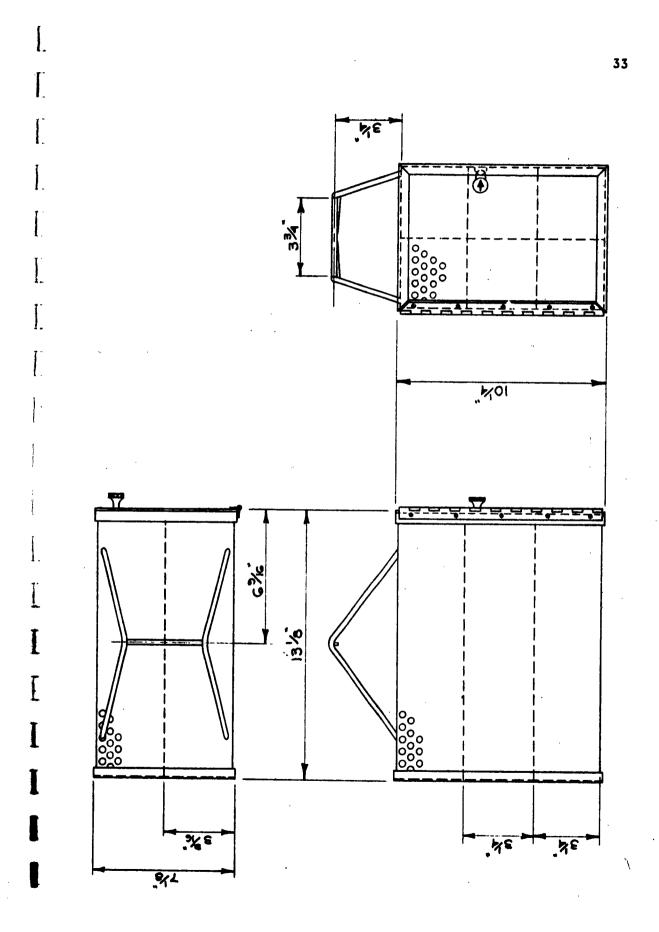


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Six gal, of water for each charge was used to maintain the water temperature below 140°F and a H₂ evolution time of 30 minutes for NaBH₄. The volume required for foam containment was determined and estimated to average about 35 cc/gm NaBH₄. Thus, for a six (6) charge run, it would require a void space of approximately 4.4 cu ft and a total volume of approximately 9.2 cu ft.

From this data, an apparatus was designed which would have a volume of 9.2 cu ft while in operation and a volume of 6.2 cu ft in the stored position. The apparatus is shown in Fig. 14 and shows the generator in an operating position. The generator as seen consists of a 20 3/4 in. ID x 15 in. high unit, which contains a stainless steel basket, Fig. 15, used to hold one (1) or up to six (6) charge canisters. The basket is held in place by brackets and is dropped into the water by a quick release mechanism which is operated by an external knob located on top of the generator. This unit is designed so that it may be placed over any size of open head drum having a 22 3/8 in. ID rolled steel edge. The generator is sealed by placing the manual lever action u-type clamp over the two drum edges and closing. A water level scale is painted on the inside of the water drum at increments of 6 gal, up to 36 gal.



CONCLUSIONS

During this quarter the preliminary design and fabrication of NaBH4 and NaAlH4 canisters and a model hydrogen generator were completed. Fifty (50) NaBH4 and fifty (50) NaAlH4 charges, each containing sufficient material to generate 45 cu ft (STP) H2 were completed and shipped to the U. S. Army Electronics Research and Development Laboratory. MSAR personnel demonstrated two NaBH4 runs using three (3) charges (or 135 cu ft of H2) in each run to U. S. Electronics Research and Development Laboratory personnel on 20 March 1963.

The major problems encountered in obtaining uniform H_2 generation has been presented by NaBH4, with NaAlH4 being much more predictable. A summation of the work conducted thus far is as follows:

- 1. Attempts to scale up small laboratory size NaBH4 experiments failed to produce the desired results. This was particularly true of surface area affects. A 4 3/4 in. cup reacted completely in 8 minutes rather than the predicted 30 minutes.
- 2. As of this report a uniform H₂ evolution rate has not been obtained; however, seeding the NaBH₄ with LiH and CoCl₂ has produced a more predictable reaction time.
- 3. Foam has been materially reduced by using a 3 in. dia. canister and a limited amount of CoCl₂. H₂ evolution may be improved with other combinations of catalysts.
- 4. Although foam has been reduced from values reported by other investigators, it continues to be a problem in large scale, 270 cu ft H₂ generations. A generator slightly larger than the AN/TMQ-3 will be required for H₂ generation of 270 cu ft.
- 5. Generation of H₂ from NaAlH4 is relatively simple in the current AN/TMQ-3 Grarator as well as the MSAR Model XI H₂ Generator designed for NaBH₄ reactions.

6. Since a reduced amount of water adversely affects the H₂ generation from NaBH₄, sufficient water is required to maintain the reaction temperatures below about 60°C. This factor also helped dictate the generator size. It had to be of sufficient size to contain the desired amount of water. There must also be sufficient free volume in the generator to prevent foaming over. Anti-foam agents other than turpentine which has proven the most effective may also be investigated since uniform H₂ generation from NaBH₄ is highly desirable.

FUTURE WORK

During the next quarter efforts to improve the NaBH4 charge will be made by using additional catalyst such as B2O3, A1Cl3 and oxallic acid in combination with CoCl2 and investigation of water soluble plastic films for containing anti-foam agents which are required for the final stages of a NaBH4 reaction when foam-over occurs will be investigated. Anti-foam agents other than turpentine which has proven the most effective may also be investigated; uniform H2 generation with NaBH4 does not make the use of anit-foam agents mandatory.

An economic evaluation of materials and the relation of NaBH4, NaAlH4 and other promising materials will be compared to CaH2 on a production basis. Large quantities of materials required in the event of a National emergency will also be considered.

Following the evaluation of the test Model XI Generator by the U. S. Electronics Research and Development Laboratory, two development model generators will be fabricated incorporating any possible revisions that would improve the generator design.

One hundred-fifty (150) NaBH4 charges will also be packaged including any revisions which will improve the charge. These are to be supplied on 31 May 1963.

Shelf life tests will continue and thus add to the information from which specifications required for storage will be determined.

A manual with directions for operating the H2 generators and descriptions of the charges supplied will be completed.

1.

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	Generation for fitten fullings backbooms, 597, 13. Generation for fitten fullings backbooms, 597, 13. THIRD QUARTERLY PROGRESS REPORT, 1 January to 1 April, 1963. [NSAR 65-61] Contract DA-56-039-5C-90699; DA Project No. 3H-36-21-004-02 (Unclassified) Large scale test using 1 to 6 charge canisters (45 cu ft H ₂ at STP/Charged Canister) were made to obtain data necessary for sizing the containers and hydrogen generator. A test hydrogen generator NSAR Hodel No. XI 50 NaBH4, canister were shipped to U. S. Army Electronics Research and Development Laboratory at Fort Nonmouth, New Jersey. Shelf life tests are continuing. Samples after three months were evaluated and early results indicate that prolonged storage of NaBH4 at elevated temperatures (50 °C) may have as prolonging effect on hydrogen evolution. There was no visible	UNCLASSIFIED 1. Balloon flights. 2. High altitude. 3. Hydrogen generation. 1. Carter, N. J. Spencer, R. A. HGGoff, M. J. 1. Contract DA-36- 039-SC-90699
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UNCLASSIFIED GENERATION FOR HIGH ALTITUDE BALLONNS. BY W. J. GENERATION FOR HIGH ALTITUDE BALLONNS. BY W. J. CERTER. T. A. SPENCET. N. J. NICCOFF. CERTER. T. A. SPENCET. N. J. NICCOFF. THIRD QUARTELY PROCEESS REPOTT, 1 January to THIRD QUARTELY PROCEESS REPOTT, 1 January to I April 1963. I April 1963. I April 1965. I High altitude. Section 234-56-21-004-02 (Unclassified) Ject No. 344-56-21-004-02 (Unclassified) Ject No. 344-56-21-04-04-04-04-04-04-04-04-04-04-04-04-04-	AD MSA Research Corporation, Callery, Fa. HYDROGEN GNEERATION FOR HIGH ALITTUDE BALLONS. JUNEAR STATION FOR HIGH ALITTUDE BALLONS. THIRD QUARTERLY PROGRESS REPORT, I January to I April 1963. I April 1963. Large scale test using 1 to 6 charge canisters (45 cu ft H2 at SPP/Charged Canister) were made to obtain data necessary for sizing the containers and hydrogen generator. A test hydrogen generator NSAR Model No. XI SO NABH, canister and 50 NaAkili, canister were shipped to U. S. Army Electronics Research and Development Laboratory at Fort Monmouth, New Jersey. Shelf life tests are continuing. Samples after three months were evaluated and early results indi- cate that prolonged storage of NaBH at elevated temperatures (50°C) may have a prolonging effect on the hydrogen evaluated and early results indi- cate that prolonged storage of NaBH at elevated difference between the NaAll4 samples at 20°C and	UNCLASSIFIED Balloon flights. High altitude. Hydrogen generation. Carter, N. J. Spener, R. A. NGOSff, M. J. Contract DA-36- 039-SC-90699

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